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**Fluid Mechanics 1**

**MCG 3340**

LAB 2 - Channel Flow

By:

**Abstract:**

The goal of this lab is to measure the pressure variation in a water flow through a channel of varying cross section. You will compare measured results to predictions made using Bernoulli's equation. We were able to prove that the Bernoulli's equation holds true even though the assumptions needed for the equation are not necessarily complete, giving us an error as we moved down the channel at a maximum of 8%.

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## Introduction:

The goal of this lab is to measure the pressure variation in a water flow through a channel of varying cross section. The measured results were compared to predictions made using Bernoulli's equation. We were able to prove that the Bernoulli's equation holds true even though the assumptions needed for the equation are not necessarily complete. The assumptions that we made to generate the equations were; . However, in this experiment we aren't able to say that these assumptions are completely true. Even though we couldn't make the assumptions we are still able to use Bernoulli's equation. At every point along the channel, the combinations of pressure and velocity will add up to the same constant proved by using the equation

$$p + \frac{1}{2}\delta v^2 + \delta gz = Const$$

This equation takes in

## Methodology:

- 1) Measure and tabulate the elevation of the top wall of the channel at the locations of the pressure taps.
- 2) Measure and tabulate the elevation of the bottom wall of the channel at the locations of the pressure taps.
- 3) Start the pump and establish a steady flow of water. Using the tank-balance apparatus, measure the flow rate. This is done by closing the drain from the fill tank, when the balance tilts, quickly add a weight to the other side of the balance and start measuring the time. When the balance tilts a second time, stop your time measurement. The amount of water added to the tank in that interval is written on the weight you added (the number on the weight applies to the water, not the weight itself). You can use these measurements to calculate the mass-flow rate of water.
- 4) With the water flowing at a known mass-flow rate, measure the height of water above the top of the channel in each pressure tap.
- 5) Repeat the procedure for a second flow rate

**Apparatus:**

This experiment is conducted in a converging-diverging channel. The channel width is 38 mm. Vertical tubes, used to measure the pressure, extend upward from small holes in the top channel wall. The position of these pressure taps are tabulated in Table 3.1. The flow is maintained by a water pump. A balance and tank are used to measure the mass flow rate of water.

**Results:**

Table 1: Measured results of flow rate 1

|                     |     |     |     |     |     |     |     |     |     |     |     |     |     |     |     |
|---------------------|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|
| Tower Height (mm)   | 163 | 162 | 161 | 160 | 158 | 155 | 153 | 153 | 163 | 164 | 165 | 162 | 163 | 163 | 164 |
| Channel height (mm) | 43  | 40  | 38  | 34  | 28  | 23  | 15  | 13  | 18  | 24  | 30  | 34  | 38  | 40  | 43  |
| Position            | O   | N   | M   | L   | K   | J   | I   | H   | G   | F   | E   | D   | C   | B   | A   |

Table 2: Measured results of flow rate 2

|                     |     |     |     |     |     |     |     |     |     |     |     |     |     |     |     |
|---------------------|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|-----|
| Tower Height (mm)   | 214 | 214 | 215 | 217 | 219 | 218 | 215 | 214 | 224 | 230 | 228 | 226 | 226 | 228 | 230 |
| Channel height (mm) | 43  | 40  | 38  | 34  | 28  | 23  | 15  | 13  | 18  | 24  | 30  | 34  | 38  | 40  | 43  |
| Position            | O   | N   | M   | L   | K   | J   | I   | H   | G   | F   | E   | D   | C   | B   | A   |

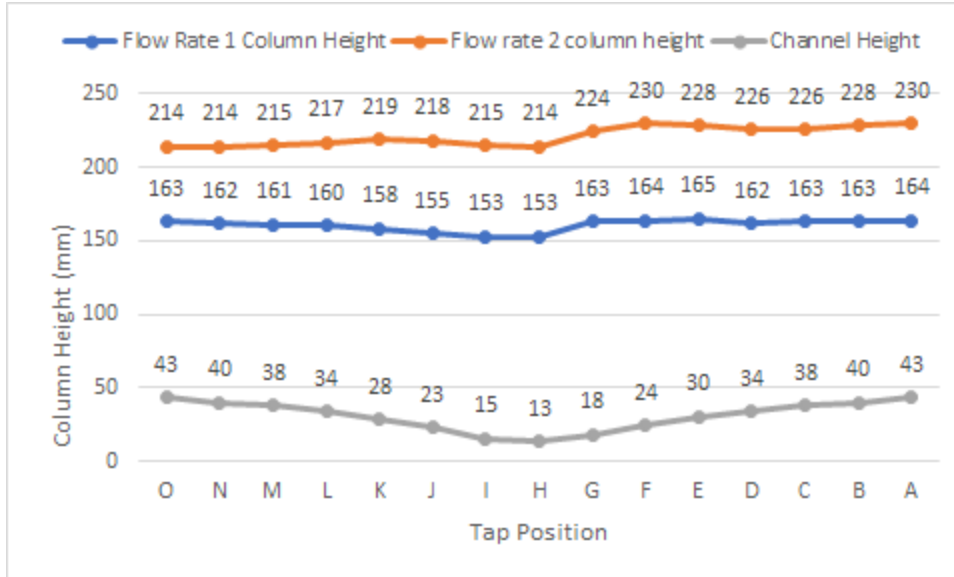


Figure 1: Tower height and Channel high relationship

Table 3: Flow Rates

| Flow test case | Flow rate (lbs/s) | Flow rate (kg/s) |
|----------------|-------------------|------------------|
| 1              | 0.976             | 0.442            |
| 2              | 0.692             | 0.314            |

Table 4: Cross sectional area at taps

|   |      |      |      |      |      |     |     |
|---|------|------|------|------|------|-----|-----|
| Cross sectional area (mm <sup>2</sup> ) | 1634 | 1520 | 1444 | 1292 | 1064 | 874 | 570 |
| Position                                | O    | N    | M    | L    | K    | J   | I   |

Table 5: Cross sectional area at taps continued

|   |     |     |     |      |      |      |      |      |
|---|-----|-----|-----|------|------|------|------|------|
| Cross sectional area (mm <sup>2</sup> ) | 494 | 684 | 912 | 1140 | 1292 | 1444 | 1520 | 1634 |
| Position                                | H   | G   | F   | E    | D    | C    | B    | A    |

## Result Calculations

Volumetric flow rate  $Q$  remains constant by  $Q = SV$  where  $S$  is the cross sectional surface area and  $V$  is the velocity of the fluid.  $Q$  can be extrapolated from the mass flow rate by  $Mass\ flow\ rate = \bar{m} = \rho Q$ . Thus the velocities at the taps can be calculated as

$$V = \frac{\bar{m}}{S\rho}$$

Pressure at taps as a function of column height =  $\rho gh$

Pressures by Bernoulli's equation.

Bernoulli's equation, assuming constant water density is  $p + \frac{1}{2}\rho v^2 + \rho gz$ . Also, all points of analysis are on the same stream line along the top of the channel. Pressure at A is assumed to be error free and is used as a reference to compare taps B through O.

The pressure for the second position is given by:

$$\frac{P_1}{\rho} + 0.5V_1^2 + gZ_1 = \frac{P_2}{\rho} + 0.5V_2^2 + gZ_2$$

$$P_2 = P_1 + 0.5\rho [V_1^2 - V_2^2] + \rho g[Z_1 - Z_2]$$

Table 6: Computed velocities and pressures

| Position | Velocity (ms <sup>-1</sup> ) |         | Column pressure (N/m <sup>2</sup> ) |         | Bernoulli pressure (N/m <sup>2</sup> ) |         | Total pressure |         |
|----------|------------------------------|---------|-------------------------------------|---------|--|---------|----------------|---------|
|          | Flow 1                       | Flow 2  | Flow 1                              | Flow 2  | Flow 1                                 | Flow 2  | Flow 1         | Flow 2  |
| A        | 0.27050                      | 0.19216 | 1608.84                             | 2256.3  | 1608.84                                | 2256.3  | 1856.34        | 2485.67 |
| B        | 0.29078                      | 0.20657 | 1599.03                             | 2236.68 | 1603.16                                | 2253.44 | 1841.63        | 2470.97 |
| C        | 0.30609                      | 0.21745 | 1599.03                             | 2217.06 | 1598.60                                | 2251.14 | 1831.83        | 2461.17 |
| D        | 0.34210                      | 0.24303 | 1589.22                             | 2217.06 | 1586.95                                | 2245.27 | 1812.23        | 2441.57 |
| E        | 0.38771                      | 0.27543 | 1618.65                             | 2236.68 | 1570.33                                | 2236.90 | 1782.83        | 2412.17 |
| F        | 0.48464                      | 0.34429 | 1608.84                             | 2256.3  | 1528.08                                | 2215.59 | 1758.33        | 2387.67 |
| G        | 0.64619                      | 0.45906 | 1599.03                             | 2197.44 | 1436.78                                | 2169.59 | 1719.13        | 2348.47 |
| H        | 0.89473                      | 0.63562 | 1500.93                             | 2099.34 | 1245.30                                | 2072.90 | 1709.33        | 2338.67 |
| I        | 0.77543                      | 0.55087 | 1500.93                             | 2109.15 | 1344.90                                | 2123.15 | 1733.83        | 2363.17 |
| J        | 0.50572                      | 0.35926 | 1520.55                             | 2138.58 | 1517.64                                | 2210.32 | 1763.23        | 2392.57 |
| K        | 0.41541                      | 0.29511 | 1549.98                             | 2148.39 | 1559.20                                | 2231.28 | 1792.63        | 2421.97 |

|   |         |         |         |         |         |         |         |         |
|---|---------|---------|---------|---------|---------|---------|---------|---------|
| L | 0.34210 | 0.24303 | 1569.6  | 2128.77 | 1586.95 | 2245.27 | 1812.23 | 2441.57 |
| M | 0.30609 | 0.21745 | 1579.41 | 2109.15 | 1598.60 | 2251.14 | 1831.83 | 2461.17 |
| N | 0.29078 | 0.20657 | 1589.22 | 2099.34 | 1603.16 | 2253.44 | 1841.63 | 2470.97 |
| O | 0.27050 | 0.19216 | 1599.03 | 2099.34 | 1608.84 | 2256.3  | 1856.34 | 2485.67 |

Error between column pressure and Bernoulli's equation pressure:

$$\text{Error \%} = |(Column Pressure - Bernoulli Pressure) / Bernoulli Pressure| * 100$$

Table 7: Error between column pressure and bernoulli's equation pressure

| Column pressure (N/m <sup>2</sup> ) |         | Bernoulli pressure (N/m <sup>2</sup> ) |         | Error % |         |
|-------------------------------------|---------|--|---------|---------|---------|
| Flow 1                              | Flow 2  | Flow 1                                 | Flow 2  | Flow 1  | Flow 2  |
| 1608.84                             | 2256.3  | 1608.84                                | 2256.3  | 0       | 0       |
| 1599.03                             | 2236.68 | 1603.16                                | 2253.44 | 0.25848 | 0.74940 |
| 1599.03                             | 2217.06 | 1598.60                                | 2251.14 | 0.02663 | 1.53739 |
| 1589.22                             | 2217.06 | 1586.95                                | 2245.27 | 0.14264 | 1.27263 |
| 1618.65                             | 2236.68 | 1570.33                                | 2236.90 | 2.98464 | 0.01007 |
| 1608.84                             | 2256.3  | 1528.08                                | 2215.59 | 5.01944 | 1.80415 |
| 1599.03                             | 2197.44 | 1436.78                                | 2169.59 | 10.1466 | 1.27002 |
| 1500.93                             | 2099.34 | 1245.30                                | 2072.90 | 17.0313 | 1.25928 |
| 1500.93                             | 2109.15 | 1344.90                                | 2123.15 | 10.3954 | 0.66407 |
| 1520.55                             | 2138.58 | 1517.64                                | 2210.32 | 0.19125 | 3.35465 |
| 1549.98                             | 2148.39 | 1559.20                                | 2231.28 | 0.59523 | 3.85830 |
| 1569.6                              | 2128.77 | 1586.95                                | 2245.27 | 1.10556 | 5.47288 |
| 1579.41                             | 2109.15 | 1598.60                                | 2251.14 | 1.21526 | 6.73233 |
| 1589.22                             | 2099.34 | 1603.16                                | 2253.44 | 0.87736 | 7.34049 |
| 1599.03                             | 2099.34 | 1608.84                                | 2256.3  | 0.61349 | 7.47663 |

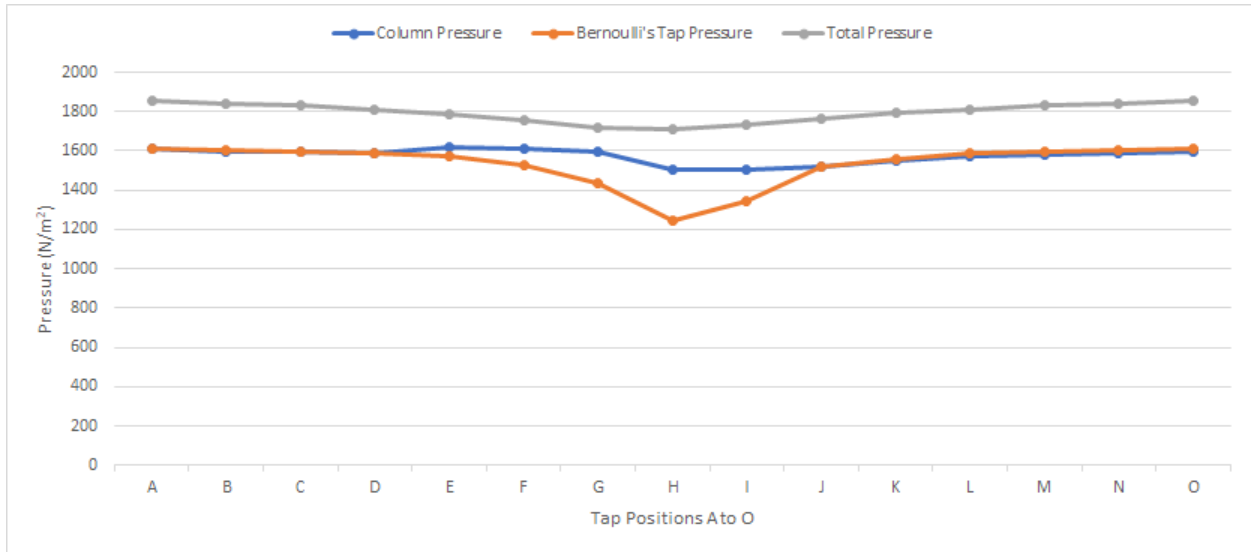


Figure 2: Pressure Graph for flow rate 1

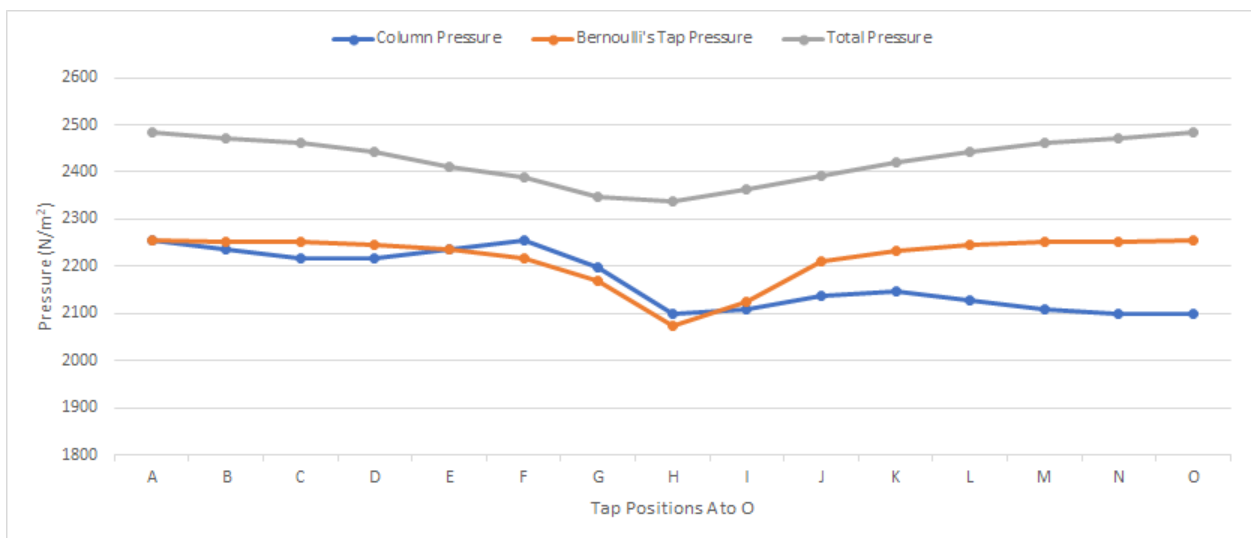


Figure 3: Pressure Graph for flow rate 2

**Discussion:**

The total pressures for both flow rates do not exhibit perfectly constant behaviours. The largest fluctuations resulted in 8% and 6% for flow rates one and two respectively. The error in these findings can be attributed to the occurrence of friction losses with the bottleneck of the channel. One possible source of experimental error is in the way we measured our finding. Most of the results were done by measuring with

very inaccurate tools. The precision of measurement tools was limited to the millimetre scale.

**Conclusion:**

In this lab we tested bernoulli's equation. We found out that even though bernoulli's equation makes the assumption of no fluid friction, the resulting error is still close enough to be used as an approximation with a maximum of 8% error. We have learned that these errors are due to pressure losses through friction of viscous fluids.