

# CVG 3116 Fall 2017

Hydraulics – Tutorial 3  
October 3, 2017

University of Ottawa



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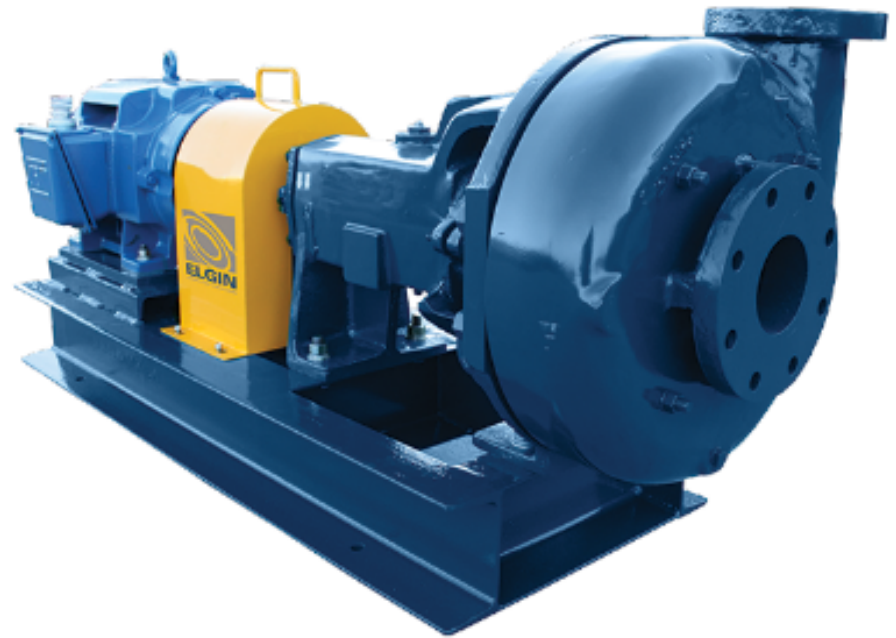
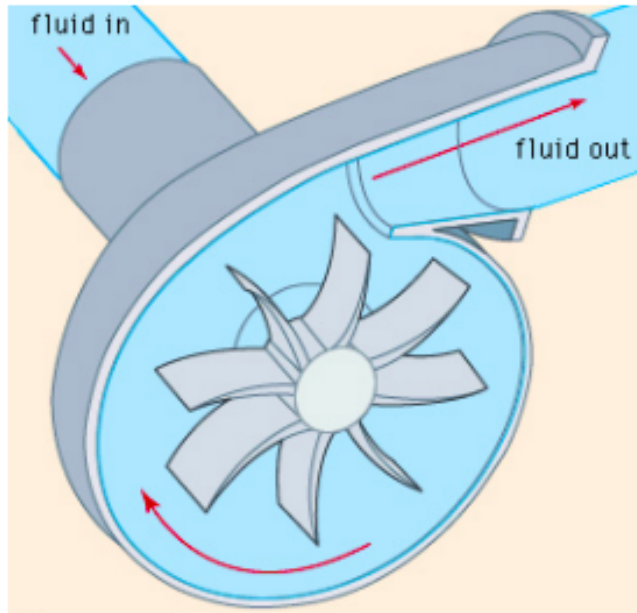
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# Lecture 4: Centrifugal (radial) pumps



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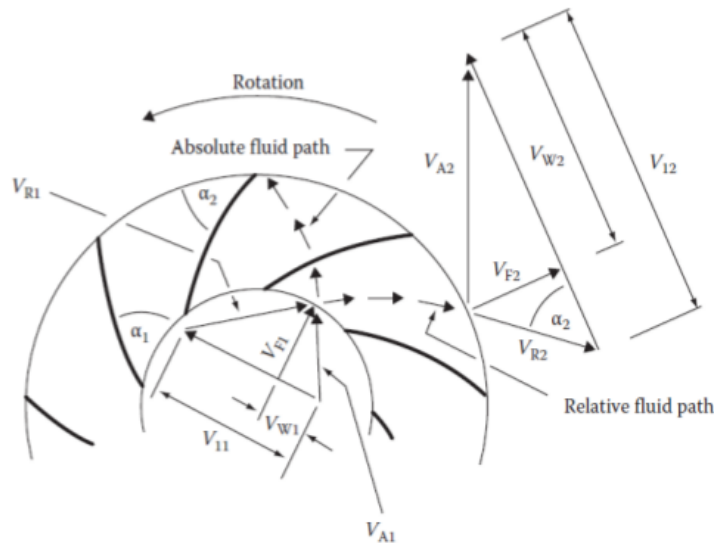


FIGURE 7.2 Velocity diagrams for centrifugal pump.

$$H_p = \eta \frac{2\pi r_2 n \left( 2\pi r_2 n - \frac{Q}{A_2} \cot \alpha_2 \right)}{g}$$

Let  $\eta$  be the hydraulic efficiency of the pump.

$$H_p = \eta H_{ideal}$$

$$H_{ideal} = \frac{power}{\rho g Q} = \frac{1}{g} (V_{W2} V_{I2} - V_{W1} V_{I1})$$

$$P = 2\pi n \rho Q (v_{W2} r_2 - v_{W1} r_1)$$

If  $V_{A1}$  is in **radial direction**, then  $V_{W1} = 0 \Rightarrow H_{ideal} = \frac{V_{W2} V_{I2}}{g}$

$V_R$ : the **relative** velocity of the fluid with respect to the impeller

$V_I$ : the **tangential** velocity of the impeller at radius  $R$  :  $V_I = 2\pi r n$

$V_A$ : the **absolute** velocity of fluid at radius  $r$

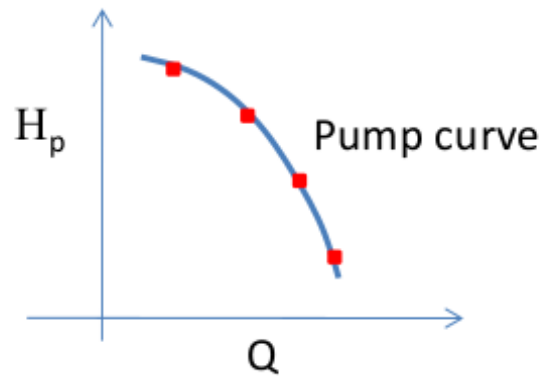
$V_W$ : the **tangential** component of  $V_A$ ; **whirl** velocity;

$V_F$ : the **radial component** of  $V_A$

$$\cot \alpha_2 = \frac{V_{I2} - V_{W2}}{V_{F2}}$$

# Lecture 5: Pumps – Pump Curve

$$H_p = \eta \frac{2\pi r_2 n \left( 2\pi r_2 n - \frac{Q}{A_2} \cot \alpha_2 \right)}{g}$$



Assume several values for  $Q$  and obtain  $H_p$  using the above formula and then plot them.

# Lecture 5: Pumps – System Curve

When you have a pump in a system, the discharge depends on the pump head. You can calculate the *discharge* based on a given *pump head* using the energy equation.

$$\frac{P_1}{\rho g} + z_1 + \frac{V_1^2}{2g} + H_p = \frac{P_2}{\rho g} + z_2 + \frac{V_2^2}{2g} + \sum (h_L + h_f)$$

$$P_1 = V_1 = P_2 = 0$$

$$z_2 - z_1 = \Delta z$$

The solution is obtained by iteration:

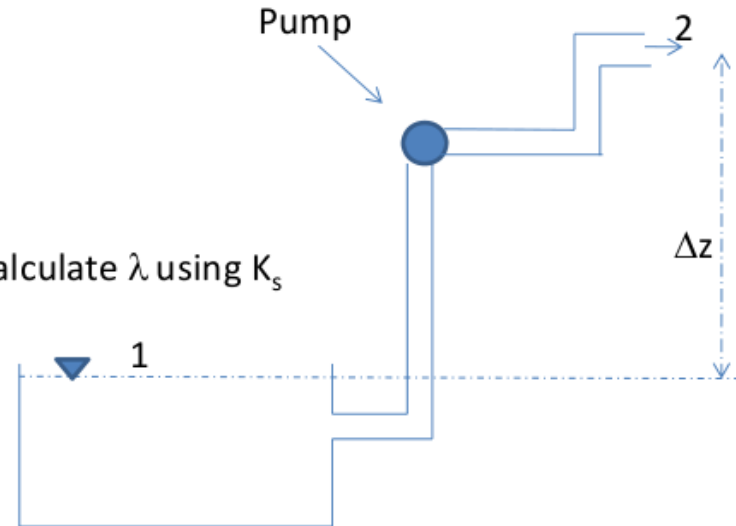
- 1- Assume the rough turbulence regime and calculate  $\lambda$  using  $K_s$
- 2- Calculate velocity

$$H_p = \Delta z + \sum \left( K_L + \frac{\lambda L}{D} \right) \frac{V_2^2}{2g}$$

- 3- Correct  $\lambda$  using Re and  $K_s$
- 4- Recalculate velocity
- 5- Continue the iteration until convergence obtained.

So you can calculate the discharge if the pump head is given.

However, in practice, **the pump head is not given** because **it depends on the discharge!**  
The relation between pump head and discharge is usually provided by the manufacturer in *pump curves*



# Lecture 5: Pumps – System Curve

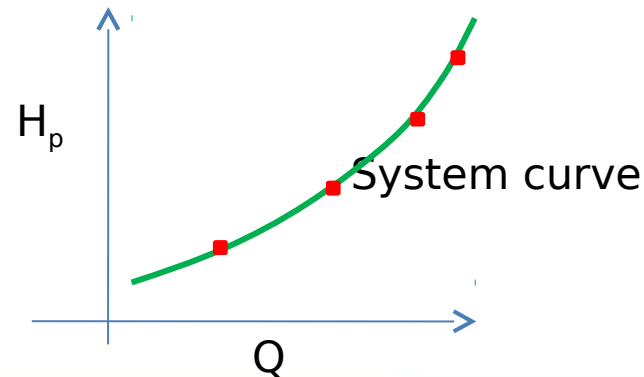
The solution procedure is as follows:

- 1 - Assume a value for the *discharge, Q*
- 2 - Calculate the *velocity in the pipe,  $V_{pipe}$*  using the continuity equation
- 3 - Calculate the *relative roughness,  $k_s/D$*  and the *Reynolds number,  $Re$*
- 4 – Determine the *friction factor,  $\lambda$*  from the Moody diagram (or Moody formula)
- 5 – Calculate *friction losses* in the pipe from the D-W equation
- 6 – Determine the *system head,  $H_{SH}$*  from:

$$H_{SH} = H_s + \left( \sum k_L + \frac{\lambda L}{D} \right) \frac{V_{pipe}^2}{2g}$$

where  $H_s = \Delta z$  – is the *static lift*.

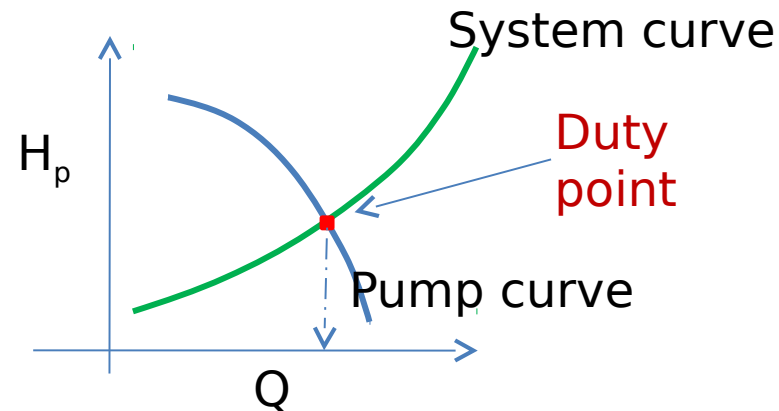
- 7 - Assume another value for the *discharge, Q* and calculate the *system head,  $H_{SH}$*  again
- 8 - *Repeat this procedure for several discharges*
- 9 - Using your results, plot the relationship between the *system head,  $H_{SH}$*  and *discharge, Q*. This plot is called the *system curve*.



# Lecture 5: Pumps – Duty point

Finally, *the discharge and the head* in the system, are given by the coordinates of the *intersection point* (also called “*duty*” *point*) of the *pump curve* and the *system curve*.

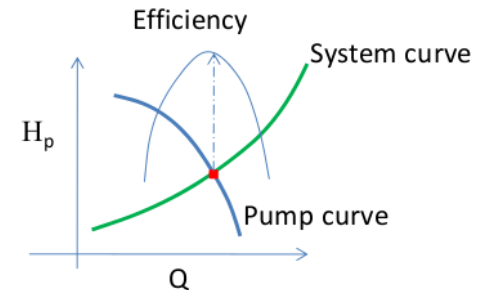
At the *duty point* the head supplied by the pump precisely matches the head requirements of the system at the same discharge.



# Lecture 5: Optimal Design

As we saw before, *the efficiency of pumps depends on the discharge.*

In order to have an optimal design, the discharge in the system must be close to the discharge at which the pump has its **maximum efficiency**:



## Pump selection

1- Calculate the *specific speed*  $N_s$ , defined as

$$N_s = NQ^{1/2} / H_p^{3/4}$$

N: rotational speed of the impeller (rev/min)

Q: Discharge in  $m^3/s$

$H_p$ : pump head in m

2- Using  $N_s$ , we can check if a pump is working close to its optimal efficiency.

i.e., the range of optimal efficiency of pumps could be identified using  $N_s$ .

Based on the value of  $N_s$ , choose the pump as following

If  $10 < N_s < 70$ , then choose centrifugal pump

If  $70 < N_s < 165$ , then choose mixed flow pump

If  $110 < N_s$  then choose axial flow

# Lecture 5: Cavitation - maximum pump elevation

1- Calculate  $N_s$

$$N_s = NQ^{1/2} / H_p^{3/4}$$

2- Calculate  $\sigma_{crit}$

$$\sigma_{crit} = \left( \frac{N_s}{191} \right)^{4/3}$$

3- Calculate  $NPSH_{crit}$

$$NPSH_{crit} = H_p \sigma_{crit}$$

4- The maximum elevation is given by

$$z < \frac{P_{atm} - P_{vap}}{\rho g} - \frac{V_{inlet}^2}{2g} - \sum (h_L + h_f) - NPSH_{crit}$$

