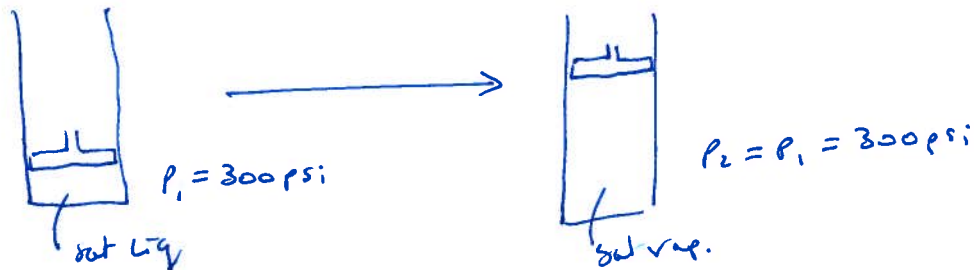


**Question I (16 Marks)**

A piston cylinder assembly initially contains saturated liquid water at 300 psi (lb<sub>f</sub>/in<sup>2</sup>).

- What is the temperature (°F) of the water? (1)
- To reach a quality of 1 at constant pressure, how much heat (Btu/lb) must be transferred? Kinetic and potential energy effects can be ignored. (5)
- Sketch the process in b. on a  $T-v$  diagram and a  $p-v$  diagram. (4)
- Using the compressibility charts, calculate the specific volume (ft<sup>3</sup>/lb) of steam at 400 psi and 500°F. (6)



From Table A-3E  $v_1 = 0.189 \text{ ft}^3/\text{lb}$   $v_2 = 1.544 \text{ ft}^3/\text{lb}$ ,  $T_1 = T_2 = 417.43^\circ\text{F}$

(a)  $T = 417.43^\circ\text{F}$

(b)  $\Delta KE + \Delta PE + \Delta U = Q - W$

$\Delta U = m \Delta u \quad \therefore \frac{Q}{m} = \Delta u + \frac{W}{m}$

$W = m \int_1^2 p \, dv \quad \frac{W}{m} = p (v_2 - v_1)$

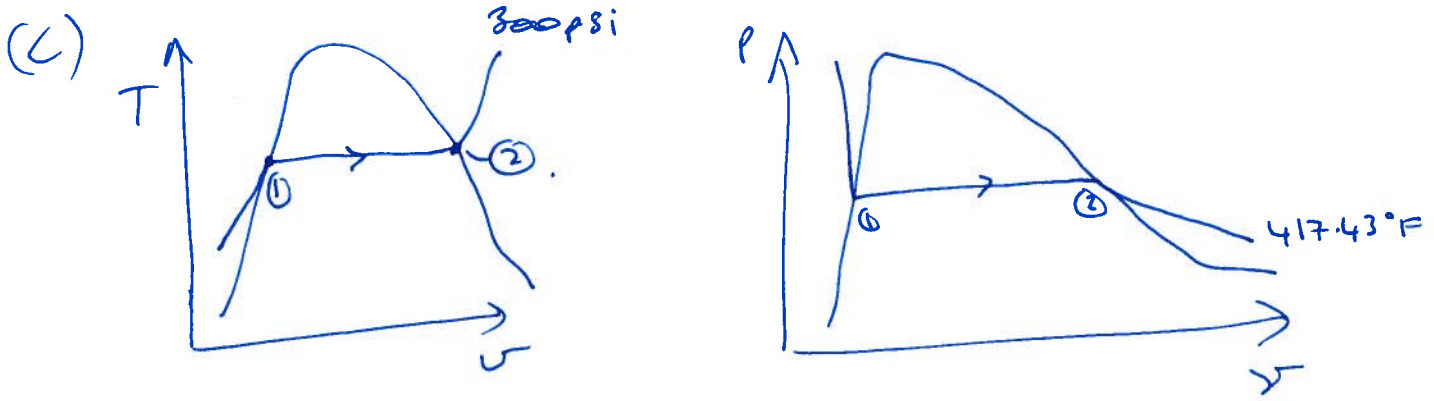
$\frac{W}{m} = 300 \frac{\text{lb}_f}{\text{in}^2} \cdot \frac{144 \text{ in}^2}{1 \text{ ft}^2} (1.544 - 0.189) \frac{\text{ft}^3}{\text{lb}} \cdot \frac{1 \text{ Btu}}{778.17 \text{ lb}_f \cdot \text{ft}}$

$\frac{W}{m} = 84.666 \text{ Btu/lb}$

$\therefore \frac{Q}{m} = \Delta u + 84.666 \frac{\text{Btu}}{\text{lb}}$

$u_2 = u_g = 1118.2 \text{ Btu/lb}$   
 $u_1 = u_f = 393.0 \text{ Btu/lb}$  } Table A-3E

$\left(\frac{Q}{m}\right) = 1118.2 - 393.0 + 84.666 = 809.9 \frac{\text{Btu}}{\text{lb}}$



(d)

$$T = 500^\circ\text{F} \quad T_c = 1165^\circ\text{R} \quad \left. \begin{array}{l} \\ \\ \end{array} \right\} \text{TABLE A-1E}$$

$$P = 400 \text{ psi} \quad P_c = 218 \text{ atm}$$

$$P_r = \frac{400 \text{ psi} \cdot \frac{1 \text{ atm}}{14.696 \text{ psi}}}{218 \text{ atm}} = 0.12$$

$$T_r = \frac{(459.67 + 500)^\circ\text{R}}{1165^\circ\text{R}} = 0.824$$

From Figure A-1  $Z = 0.92$

$$v = \frac{ZRT}{P} \quad R = \frac{1545 \frac{\text{ft} \cdot \text{lb}_f}{\text{lbmol} \cdot ^\circ\text{R}}}{18.02 \text{ lb/lbmol}}$$

(Table A-1E)

$$v = \frac{0.92 \cdot \left(\frac{1545}{18.02}\right) \frac{\text{ft} \cdot \text{lb}_f}{\text{lb} \cdot ^\circ\text{R}} \cdot 959.67^\circ\text{R}}{400 \frac{\text{lb}_f}{\text{in}^2} \cdot \frac{144 \text{ in}^2}{\text{ft}^2}}$$

$$v = 1.314 \frac{\text{ft}^3}{\text{lb}}$$

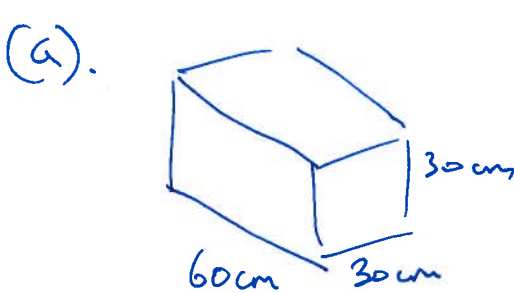
(compare to Table A-4E)

$$v = 1.284 \frac{\text{ft}^3}{\text{lb}}$$

**Question Number II (16 Marks)**

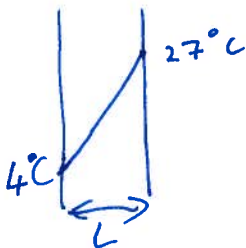
Consider an insulated cooler that has internal dimensions of 60 cm wide, 30 cm deep, and 30 cm high. The walls are 2 cm thick with a thermal conductivity of 0.05 W/(m K). The cooler is left in the sun and gradually warms up so that the outside surface of the cooler is at a temperature of 27°C.

- When the temperature in the cooler is 4°C, what is the rate of heat transfer (W) between the four sides of the cooler and the environment? Use the internal dimensions to calculate the area. (5)
- If a device (e.g., chiller) could be attached to keep the cooler at 4°C, how much work (kJ) would the system do if the total heat transfer is 100 kJ? (Hint: clearly state what the system is.) (3)
- What is the heat capacity (kJ/(kmol K)) of the air surrounding the cooler (i.e., at 27°C)? (2)
- What force of friction (N) is required to prevent the top from popping off the cooler once the air inside the cooler reaches 27°C? For this question, assume that the cooler contains only air which cannot escape, the top of the cooler has a mass of 500 g and an area of 0.18 m<sup>2</sup>, the atmospheric pressure is 0.89 bar,  $g$  is 9.81 m/s<sup>2</sup>, and the air behaves like an ideal gas. (6)



$$\text{Area} = \left[ (0.6 \times 0.3 \times 2) + (0.3 \times 0.3 \times 2) \right] \text{m}^2$$

$$A = 0.54 \text{ m}^2.$$



$$Q = -k \cdot A \cdot (T_{in} - T_{out})$$

$$= -0.05 \frac{\text{W}}{\text{mK}} \cdot 0.54 \text{ m}^2 (4 - 27) \text{ K}$$

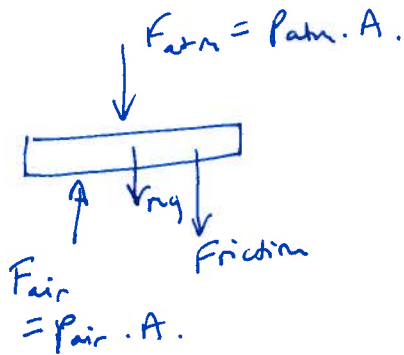
$$= 31.05 \text{ W}$$

(b) Cooler is the system. Cooler at const. temp. so  $\Delta u = 0$ . Also  $\Delta KE = \Delta PE = 0$ .  
 So  $Q = W = -100 \text{ kW}$  ie work is added to the cooler, heat is removed.

(c) Table A-20  $T = 300 \text{ K}$   $C_p = 1.005 \frac{\text{kJ}}{\text{kgK}} \times 28.97 \frac{\text{kg}}{\text{kmol}}$

$$C_p = 29.11 \frac{\text{kJ}}{\text{kmolK}}$$

(a) Force balance on lid:



$$P_1 \frac{V_1}{T_1} = P_2 \frac{V_2}{T_2}$$

$$\frac{P_2}{P_1} = \frac{T_2}{T_1} \therefore P_2 = P_1 \left( \frac{T_2}{T_1} \right)$$

assuming  $P_1 = P_{atm} = 0.89 \text{ bar}$

$$P_2 = 0.89 \text{ bar} \cdot \frac{300 \text{ K}}{277 \text{ K}} = 0.964 \text{ bar}$$

$$F_{\text{friction}} = F_{\text{air}} - F_{\text{atm}} - mg$$

$$= A(P_{\text{air}} - P_{\text{atm}}) - mg$$

$$= 0.18 \text{ m}^2 (0.964 - 0.89) \text{ bar} \cdot \frac{10^5 \text{ N/m}^2}{1 \text{ bar}} - 0.5 \text{ kg} \cdot 9.81 \frac{\text{m}}{\text{s}^2}$$

$$= \underline{\underline{1327 \text{ N}}}$$

**Question Number III (18 marks)**

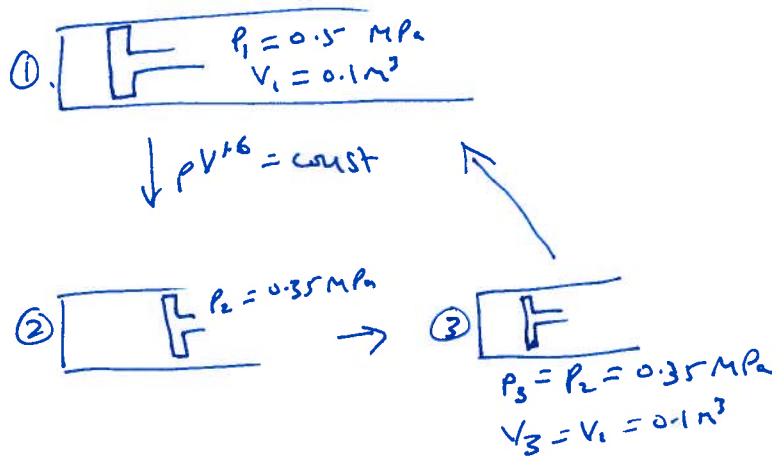
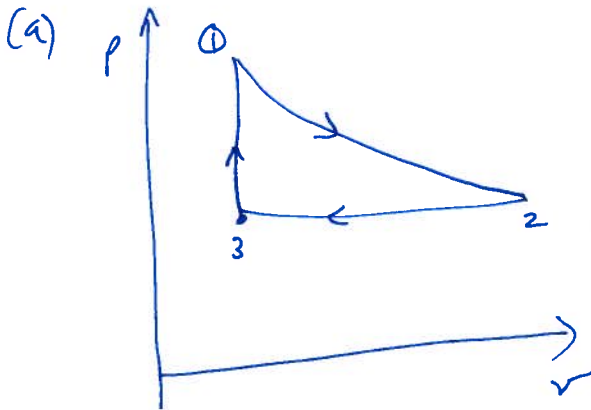
A piston-cylinder assembly contains carbon dioxide (CO<sub>2</sub>). The CO<sub>2</sub> undergoes a power cycle consisting of three processes in series:

Process 1-2: Polytropic expansion with  $n = 1.6$  from  $p_1 = 0.5$  MPa to  $p_2 = 0.35$  MPa,  $V_1 = 0.1$  m<sup>3</sup>

Process 2-3: Isobaric compression to  $V_1$ .

Process 3-1: Constant volume heating.

- Sketch the processes on a  $p$ - $V$  diagram. (4)
- Calculate  $W_{12}$  (kJ). (5)
- Calculate  $Q_{cycle}$  (kJ). (4)
- If the pressure at state 1 was measured with a pressure gauge that had divisions of 10 kPa, what is the uncertainty in this pressure? (1)
- The temperature is calculated at state 1 using the ideal gas law;  $v = 10$  L/mol  $\pm$  0.1 L/mol. What are the temperature ( $^{\circ}$ C) and its uncertainty? (4)



(b)

$$W_{12} = \frac{p_2 V_2 - p_1 V_1}{1 - n}$$

$$p_2 V_2^{1.6} = p_1 V_1^{1.6}$$

$$V_2 = V_1 \cdot \left(\frac{p_1}{p_2}\right)^{\frac{1}{1.6}} = 0.1 \text{ m}^3 \cdot \left(\frac{0.5}{0.35}\right)^{\frac{1}{1.6}}$$

$$V_2 = 0.125 \text{ m}^3$$

$$W_{12} = \frac{0.35 \cdot 10^6 \frac{\text{N}}{\text{m}^2} \cdot 0.125 \text{ m}^3 - 0.5 \cdot 10^6 \frac{\text{N}}{\text{m}^2} \cdot 0.1 \text{ m}^3}{1 - 1.6}$$

$$W_{12} = 10417 \text{ J} \approx \underline{10.42 \text{ kJ}}$$

(c)

$$Q_{cy.} = W_{cy.} = W_{12} + W_{23} + W_{31}$$

$$W_{23} = p(V_3 - V_2)$$

$$= 0.35 \cdot 10^6 \frac{\text{N}}{\text{m}^2} \cdot (0.1 \text{ m}^3 - 0.125 \text{ m}^3)$$

$$Q_{cy.} = (10417 - 8750) = 1667 \text{ J}$$

$$= \underline{1.67 \text{ kJ}}$$

$$W_{23} = -8750 \text{ J}$$

(d) Uncertainty =  $\pm$  half increment.  
 =  $\pm 5 \text{ kPa}$ .

(e)  $T = \frac{pV}{R} = \frac{0.5 \cdot 10^6 \frac{\text{N}}{\text{m}^2} \cdot 10 \frac{\text{m}^3}{\text{kmol}}}{8.314 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}} \cdot \frac{1000 \text{ J}}{\text{kJ}}}$   
 $T = 601.4 \text{ K}$ .

$$\left(\frac{W_T}{T}\right)^2 = \left(\frac{W_p}{p}\right)^2 + \left(\frac{W_V}{V}\right)^2$$

$$\left(\frac{W_T}{601 \text{ K}}\right)^2 = \left(\frac{5 \text{ kPa}}{500 \text{ kPa}}\right)^2 + \left(\frac{0.1 \text{ m}^3/\text{kmol}}{10 \text{ m}^3/\text{kmol}}\right)^2$$

$$W_T = \pm (601 \sqrt{0.0002}) \text{ K}$$

$$= \pm 8.5 \text{ K} = \pm 8.5^\circ \text{C}$$

$$T = (601.4 - 273.15) \pm 8.5^\circ \text{C}$$

$$T = 328 \pm 8.5^\circ \text{C}$$